

GEOTHERMAL POWER PLANT CYCLES AND MAIN COMPONENTS

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ABSTRACT

The following text is covering the basic principles of thermodynamics to be treated in lectures “Steam cycles for geothermal power production”, “Design of the main components of a steam cycle power plant”, “Binary cycles for geothermal power production” and “Design of the main components of a binary cycle power plant”.

1. INTRODUCTION

Geothermal power plants can be divided into two main groups, steam cycles and binary cycles. Typically the steam cycles are used at higher well enthalpies, and binary cycles for lower enthalpies. The steam cycles allow the fluid to boil, and then the steam is separated from the brine and expanded in a turbine. Usually the brine is rejected to the environment (re-injected), or it is flashed again at a lower pressure. Here the Single Flash (SF) and Double Flash (DF) cycles will be presented.

A binary cycle uses a secondary working fluid in a closed power generation cycle. A heat exchanger is used to transfer heat from the geothermal fluid to the working fluid, and the cooled brine is then rejected to the environment or re-injected. The Organic Rankine Cycle (ORC) and Kalina cycle will be presented.

2. SINGLE FLASH

A flow sheet for the SF cycle is shown in Figure 1. The geothermal fluid enters the well at the source inlet temperature, station *1*. Due to the well pressure loss the fluid has started to boil at station *2*, when it enters the separator. The brine from the separator is at station *3*, and is re-injected at station *4*, the geothermal fluid return condition. The steam from the separator is at station *5*, where the steam enters the turbine. The steam is then expanded through the turbine down to station *6*, where the condenser pressure prevails.

The condenser shown here is air cooled, with the cooling air entering the condenser at station *c1* and leaving at station *c2*. The condenser hot well is at station *7*. The fluid is re-injected at station *4*.

Typically, such a process is displayed on a thermodynamic T-s diagram, where the the temperature in the cycle is plotted against the entropy (Figure 2). The condition at station *1* is usually compressed liquid. In vapour dominated fields, such as Lardarello in Italy, the inflow is in the wet region close to the vapour saturation line.

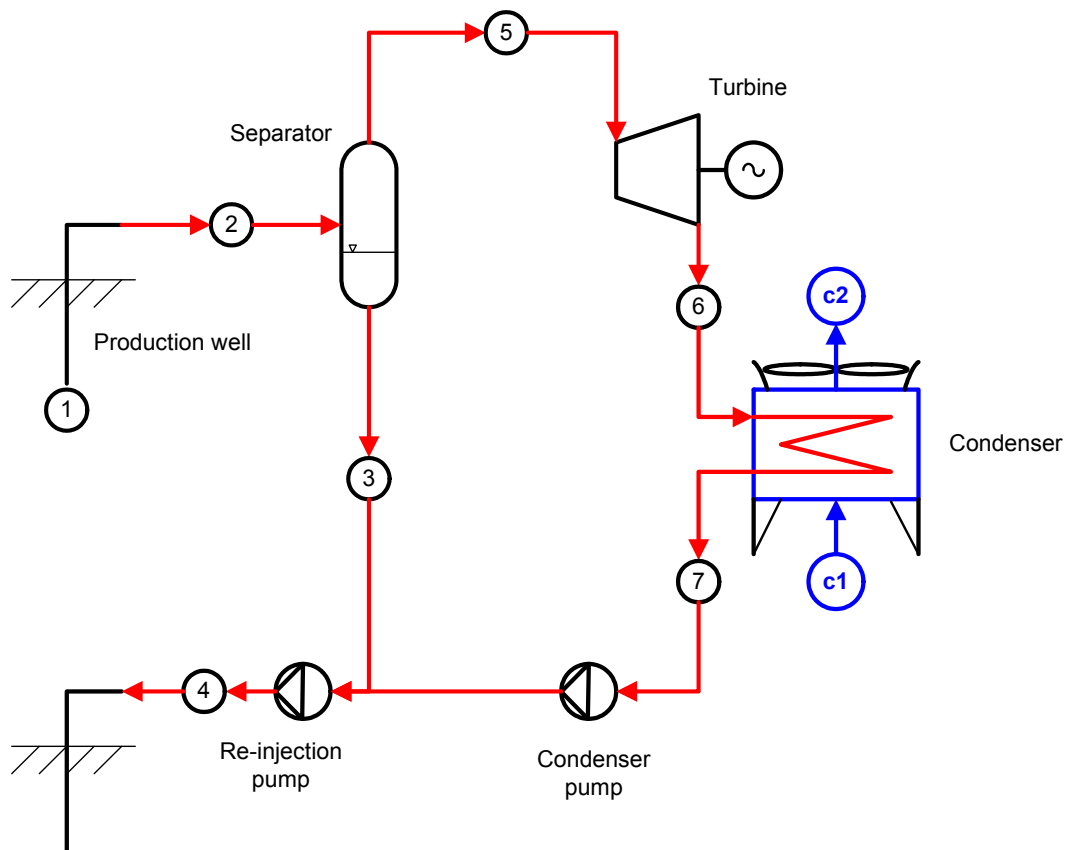


FIGURE 1: Single flash cycle schematic

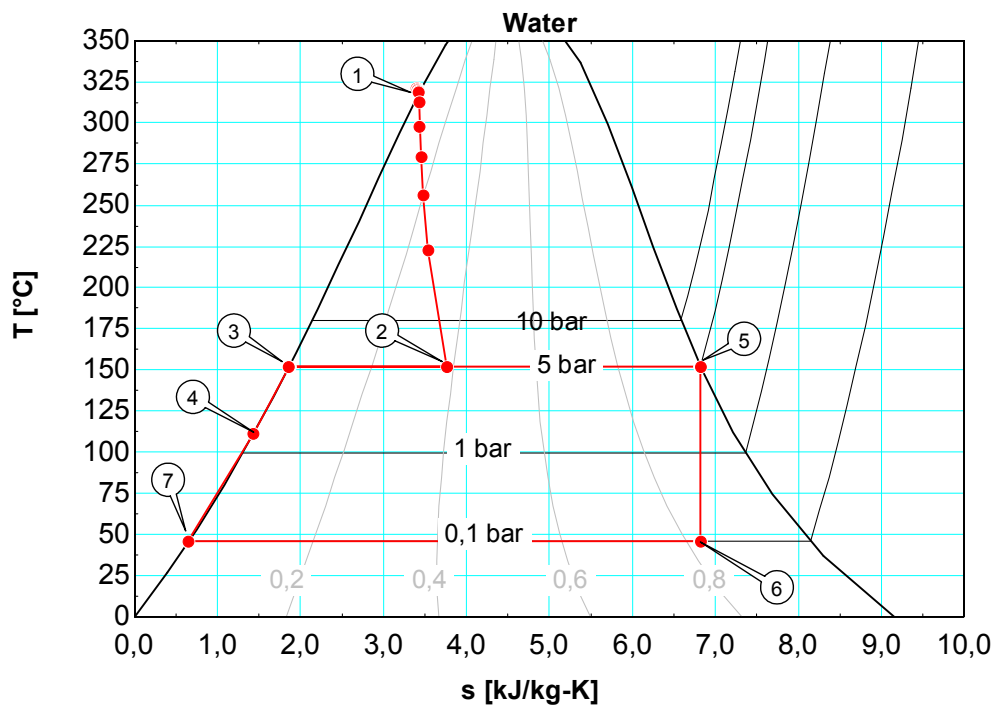


FIGURE 2: T-s diagram of a single flash cycle

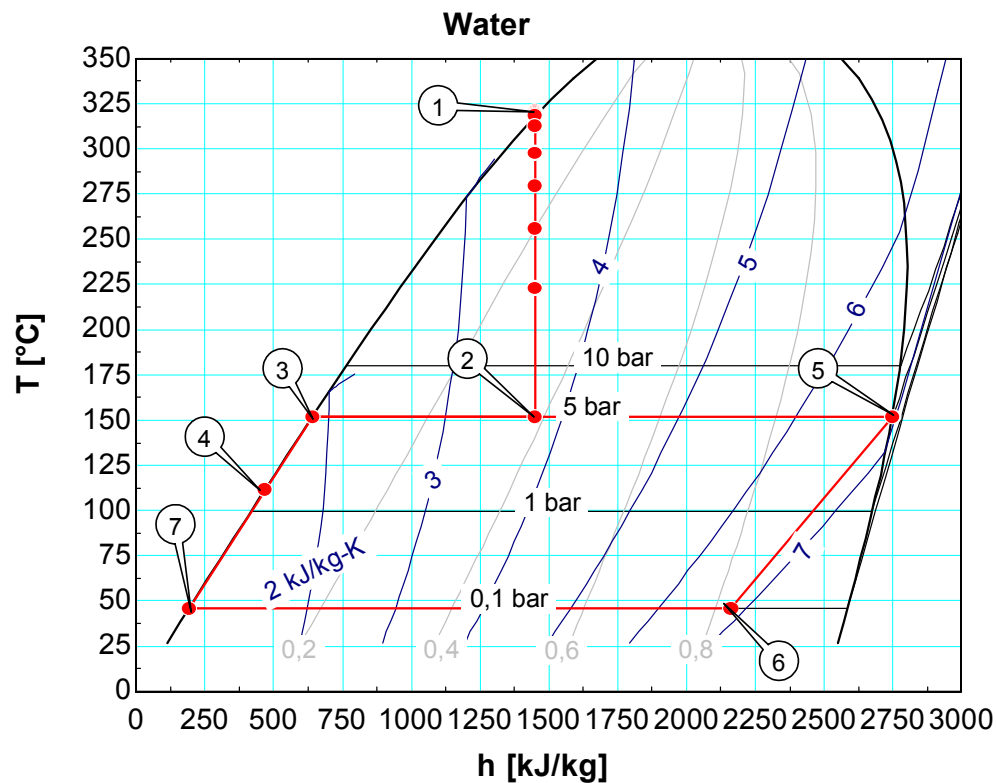


FIGURE 3: T-h diagram of a single flash cycle

3. DOUBLE FLASH

A flow sheet for the DF cycle is shown in Figure 4. The geothermal fluid enters the well at the source inlet temperature, station 1. Due to the well pressure loss the fluid has started to boil at station 2, when it enters the separator. The brine from the separator is at station 3, and is throttled down to a lower pressure level at station 8. The partly boiled brine is then led to a low pressure separator, where the steam is led to the turbine at station 9. The turbine is designed in such a way, that the pressure difference over the first stages is the same as the pressure difference between the high and low pressure separators. The mass flow in the lower pressure stages of the turbine is then higher than in the high pressure stages, just the opposite of what happens in a traditional fuel fired power plant with a bleed for the feedwater heaters from the turbine.

The brine from the low pressure separator is at station 10, and is then re-injected at station 4, the geothermal fluid return condition.

The steam from the high pressure separator is at station 5, where the steam enters the turbine. The low pressure steam enters the turbine a few stages later, at station 9. The steam is then expanded through the turbine down to station 6, where the condenser pressure prevails.

The condenser shown here is air cooled, with the cooling air entering the condenser at station *c1* and leaving at station *c2*.

The condenser hot well is at station 7. The fluid is re-injected at station 4.

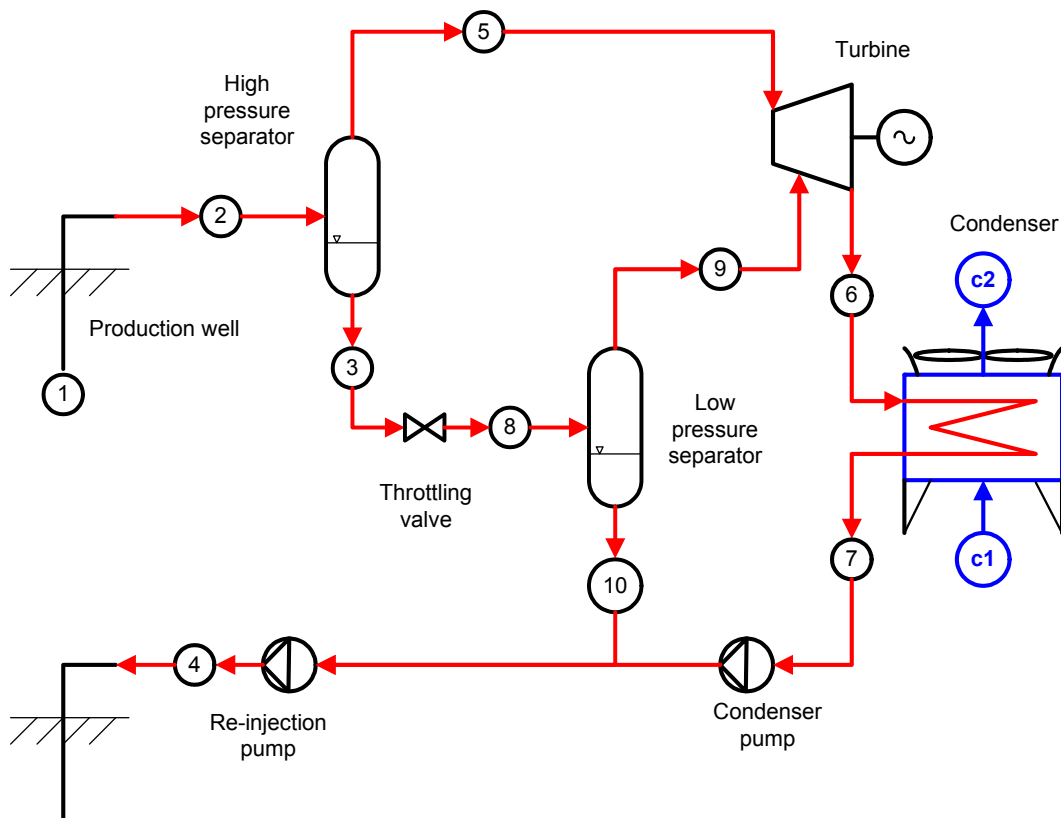


FIGURE 4: Double flash cycle schematic

The double flash cycle is presented in Figure 5 on a T-s diagram and on a T-h diagram in Figure 6.

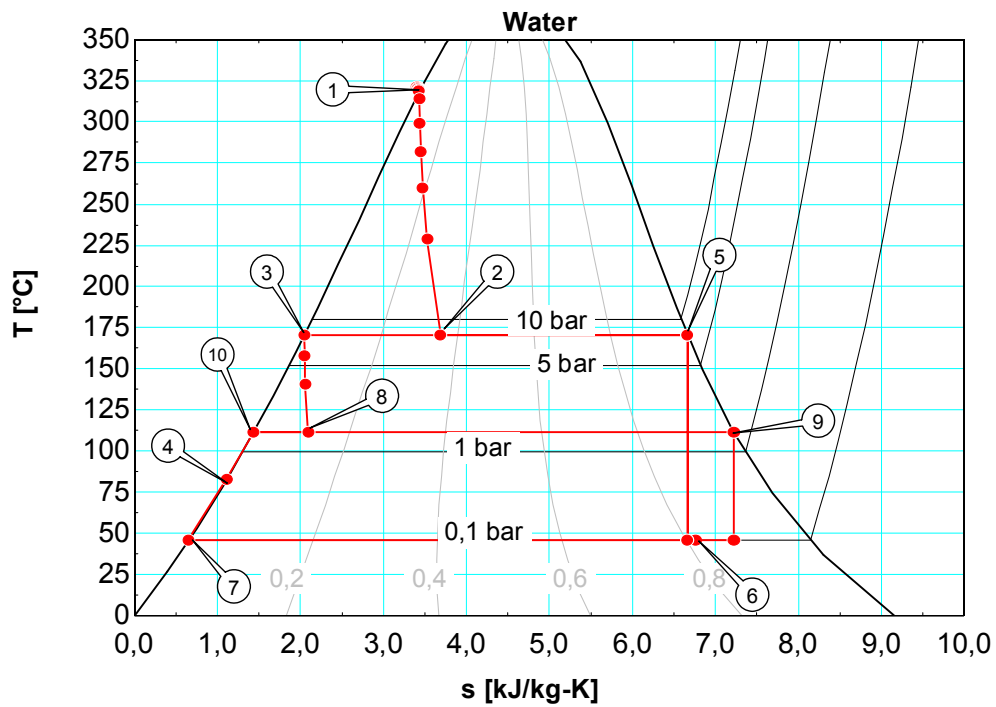


FIGURE 5: T-s diagram of a double flash cycle

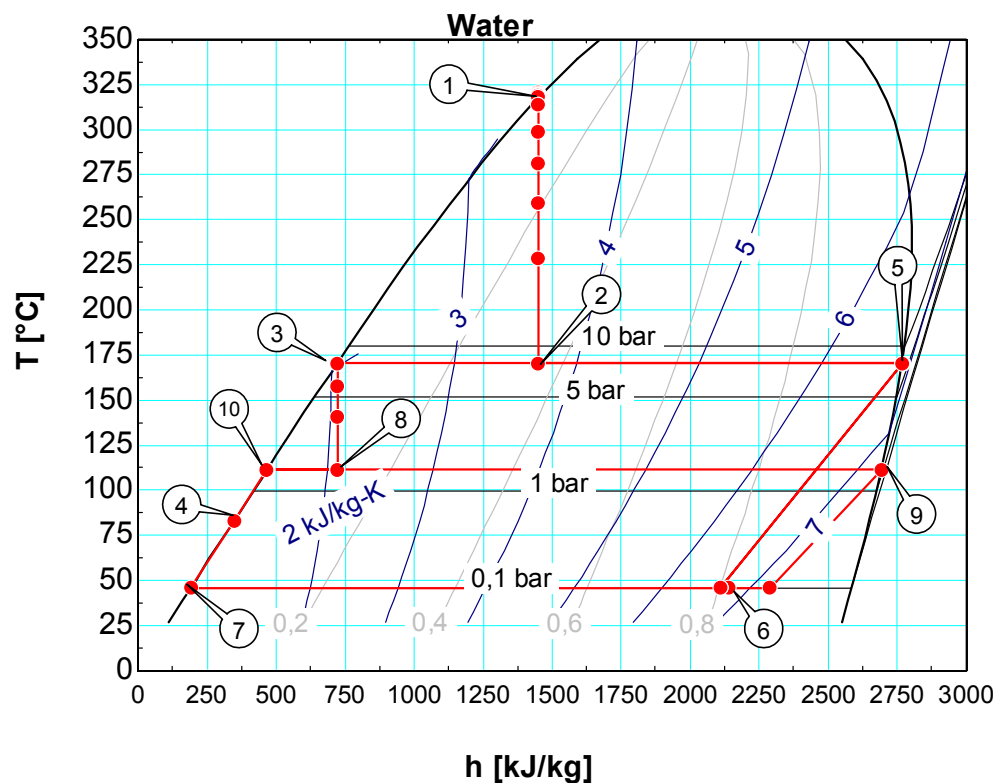


FIGURE 6: T-h diagram of a double flash cycle

4. ORGANIC RANKINE CYCLE (ORC)

A flow sheet for the ORC cycle is shown in Figure 7. The geothermal fluid enters the well at the source inlet temperature, station $s1$. The fluid is frequently liquid water. If the pressure is kept sufficiently high, no non-condensable gases will be separated from the liquid, and a gas extraction system is not necessary. The fluid is then cooled down in the vaporizer, and sent to re-injection at station $s2$.

The ORC with regeneration is presented in Figure 8 on a T-s diagram and on a T-h diagram in Figure 9.

Pre-heated (in the regenerator) ORC fluid enters the vaporizer at station 2. The fluid is heated to saturation in the vaporizer, or even with superheat in some cases. The vapour leaves the vaporizer at station 3, and enters the turbine.

The exit vapour from the turbine enters the regenerator at station 4, where the superheat in the steam can be used to pre-heat the condensed fluid prior to vaporizer entry. The now cooled vapour enters the condenser at station 5, where it is condensed down to saturated liquid at station 6.

A circulation pump raises the pressure from the condenser pressure up to the high pressure level in station 1. There the fluid enters the regenerator for pre-heat before vaporizer entry.

The condenser shown here is air cooled, with the cooling air entering the condenser at station $c1$ and leaving at station $c2$.

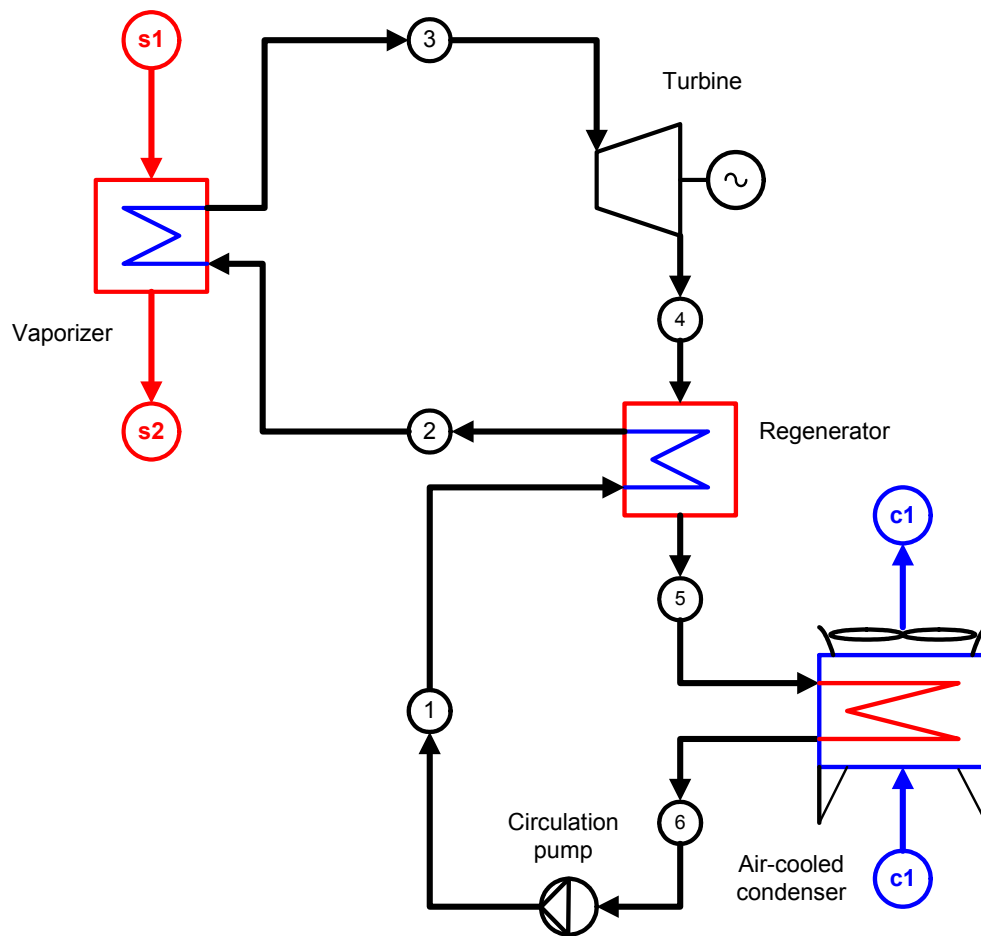


FIGURE 7: Flow diagram for an ORC cycle with regeneration

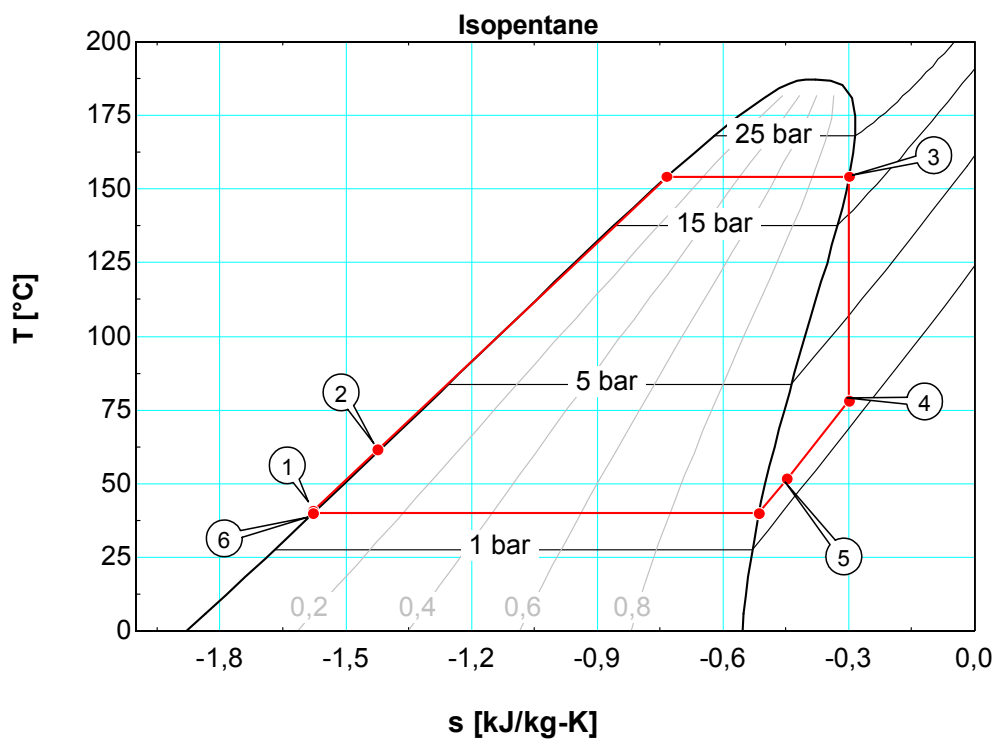


FIGURE 8: T-s diagram of an ORC cycle with regeneration

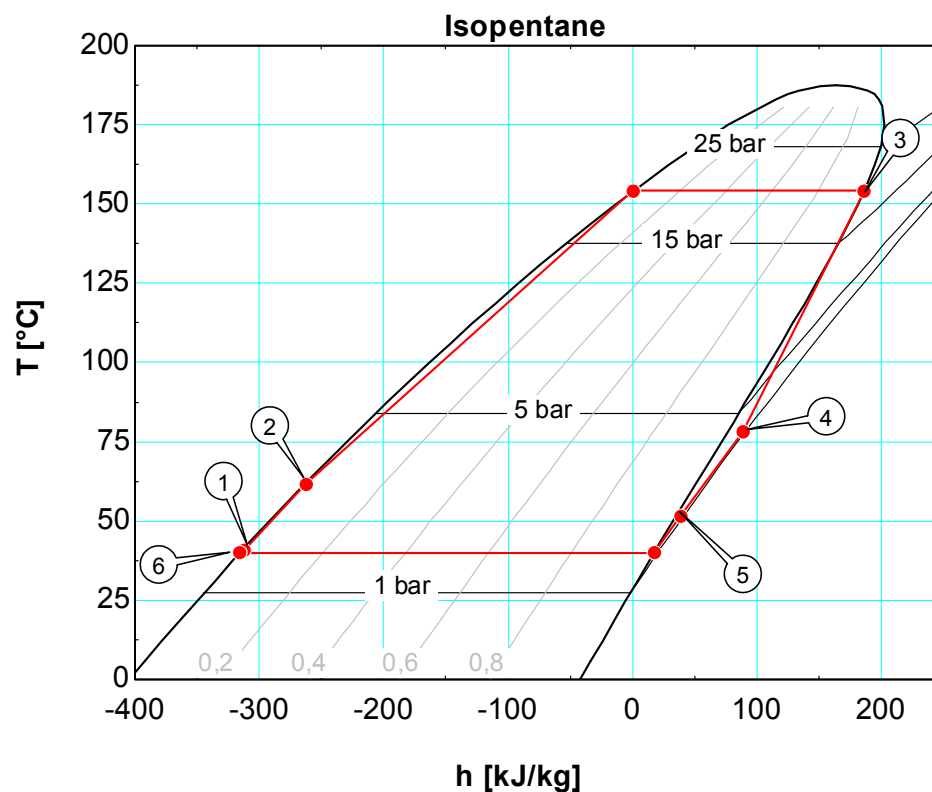


FIGURE 9: T-h diagram of an ORC cycle with regeneration

5. REGENERATION

Regeneration will increase the power plant efficiency. Then a part of the rejected heat is recovered for input to the power plant. If the plant were run on fuel, this would lead to direct fuel savings. This is not the case in geothermal power production. There the wells have certain maximum flow rate, and the well cost is usually entirely fixed, has very little if any relation to the flow from the well. The more the fluid from the well can be cooled, the more heat can be input to the power plant.

Regeneration increases the temperature of the working fluid at the vaporizer entry, and leads thus to higher geothermal fluid exit temperature from the vaporizer. The heat removal from the geothermal fluid is thus partly replaced by the recovered heat.

There is frequently a lower temperature limit on the geothermal fluid temperature. This limit may be imposed by chemistry (danger of scaling) or the requirements of a secondary process, such as district heating. If this is the case, regeneration can help.

Figure 10 shows a calculation of an isopentane ORC cycle, with geothermal fluid temperature of 200°C. It is assumed that the well flow is 1 kg/s, condensation temperature is 40°C. Three curves are calculated, no regeneration at all, if 50% of the heat available is used for regeneration and finally if all the available heat is used. The available heat is the heat which can be removed from the turbine exit vapour until the vapour reaches dew point. After that the vapour temperature is the same as the condensation temperature and no regeneration can occur. Note that the following calculation results are based on an ideal ORC cycle.

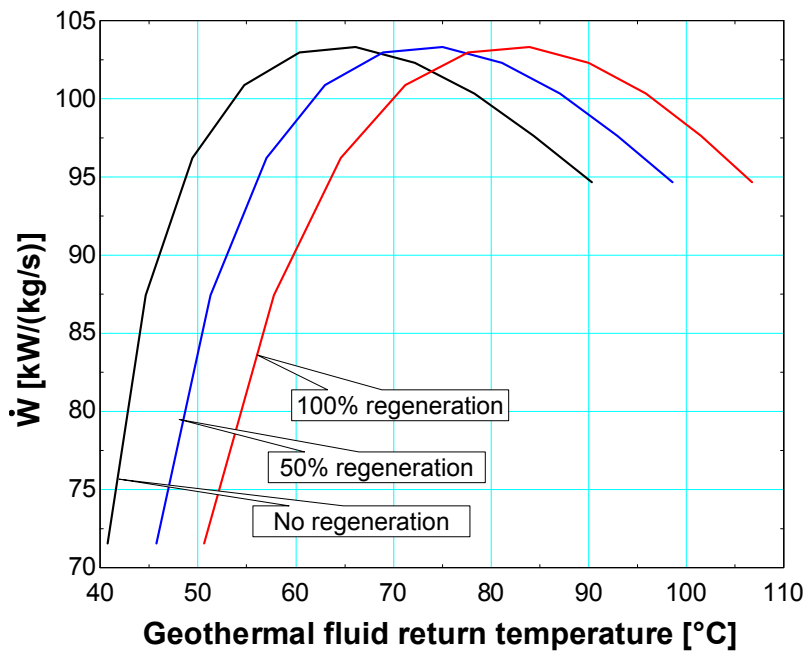


FIGURE 10: Power obtained from 1 kg/s of 200°C geothermal fluid (ideal cycle)

It can be seen from Figure 10, that the point of highest power is moved upwards by ca 20°C by the effect of the regeneration. Regeneration can thus keep the maximum power for geothermal fluid temperatures from ca 65°C to ca 85°C. It has to be kept in mind that a regenerator will be large and expensive, as well as causing pressure drop and associated losses. A cycle without regeneration will be more economical, if the geothermal fluid does not have any temperature limitation. Regeneration will not, repeat not, increase the produced power, even if it increases the efficiency. The increase of efficiency results only from less input of heat from the geothermal fluid. And this heat is normally free of charge.

The thermal efficiency increases when the geothermal return temperature increases (Figure 11). This is in accordance with the second law of thermodynamics, as the average input temperature of the heat increases, and thereby the efficiency.

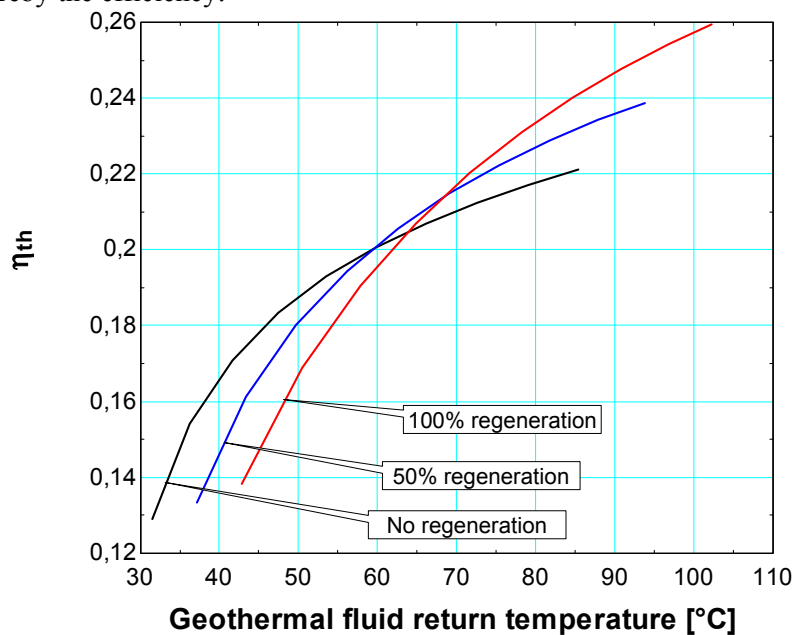


FIGURE 11: Thermal power plant efficiency (ideal cycle)

The power plant effectiveness is independent of the regeneration ratio, if the effectiveness is drawn as a function of the geothermal return temperature (Figure 12). And obviously this is a linear relation of the return temperature.

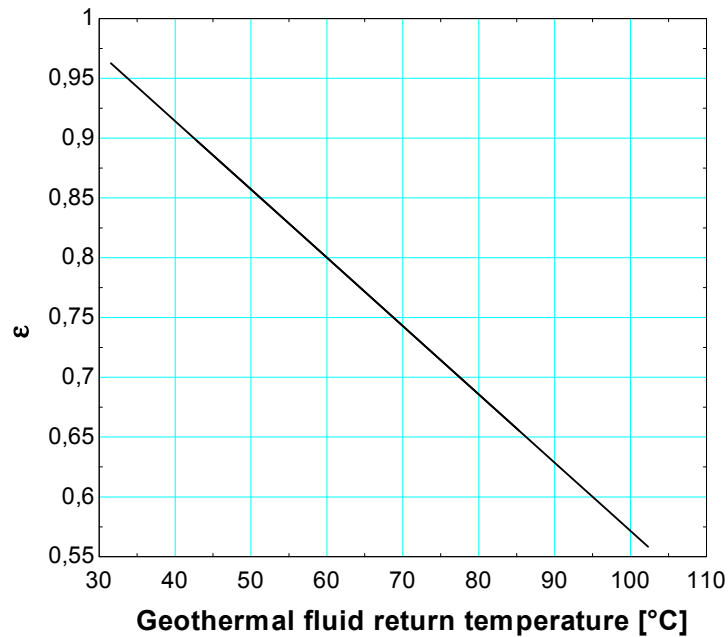


FIGURE 12: Power plant effectiveness (ideal cycle)

The total efficiency is found by multiplying the thermal efficiency by the effectiveness (Figure 13), and logically this is the same set of curves as the curves for the power obtained from the geothermal flow at the very beginning.

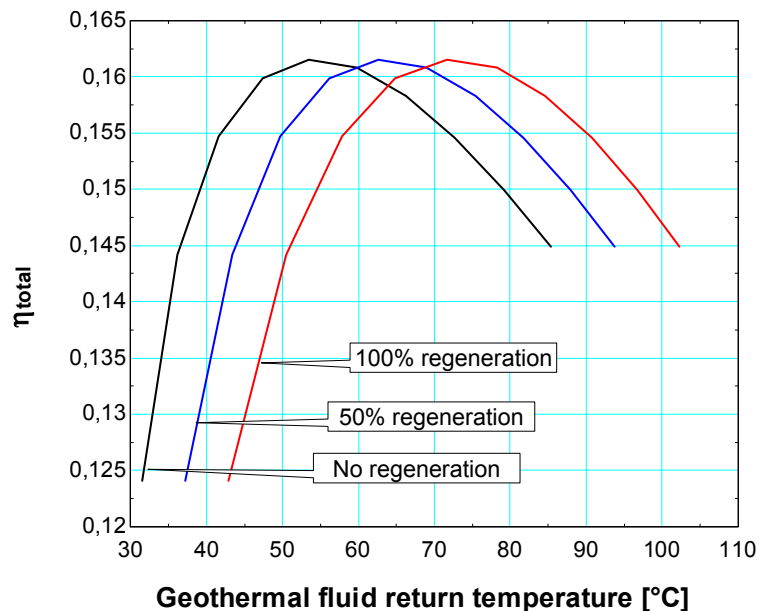


FIGURE 13: Thermal power plant total efficiency (ideal cycle)

The conclusion is simply that regeneration serves only to move the highest power production towards higher geothermal return temperature.

A final note is that a real cycle will show lower efficiency for higher regeneration, so regeneration will always reduce the maximum power available from a given geothermal flow stream. Regeneration will as well increase the plant cost, and has thus to be seen as a measure to preserve power, if a secondary process or geothermal fluid chemistry limits the return fluid temperature.

6. KALINA

The Kalina cycle is patented by the inventor, Mr Alexander Kalina. There are quite a few variations of the cycle. The Kalina power generation cycle is a modified Clausius-Rankine cycle. The cycle is using a mixture of ammonia and water as a working fluid. The benefit of this mixture is mainly that both vaporization and condensation of the mixture happens at a variable temperature. There is no simple boiling or condensation temperature, rather a boiling temperature range as well as condensation range. This is due to the fact, that the phase change process is a combined process, both the phase change of the substance and absorption/separation of ammonia from water.

6.1 The fluid

A phase diagram for ammonia – water mixture at 30 bar pressure is shown in Figure 14. The lower curve is the so-called bubble curve, when the first vapour bubble is created. This bubble has higher ammonia content than the boiling liquid. As the bubble ammonia content is higher than that of the liquid, the ammonia content in the liquid phase will be reduced. The upper curve is the so-called dew curve, when the last liquid drop evaporates. This drop has considerably lower ammonia content than the vapour.

The boiling process for 50% mixture is indicated in Figure 14.

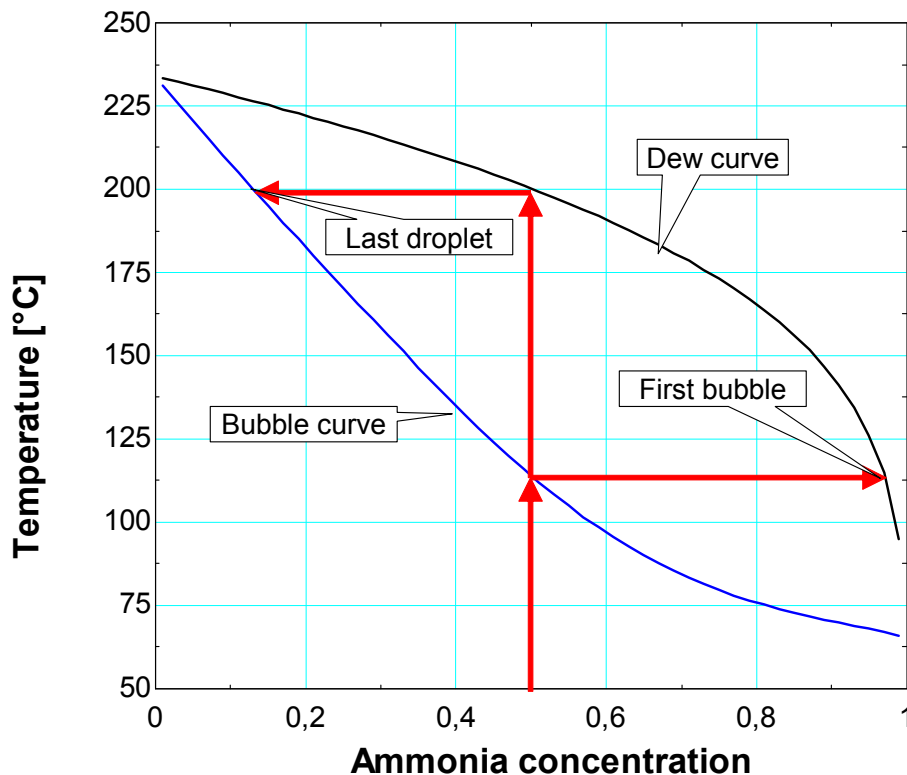


FIGURE 14: Ammonia-water phase diagram at 30 bar pressure

The temperature range for the boiling of the mixture at 30 bar is shown in Figure 15. The temperature range from bubble to dew is largest at approximately 67% ammonia concentration, and is then close to 95°C.

The mixture has thus a finite heat capacity, which is beneficial if the heat source is a liquid with constant or close to constant heat capacity.

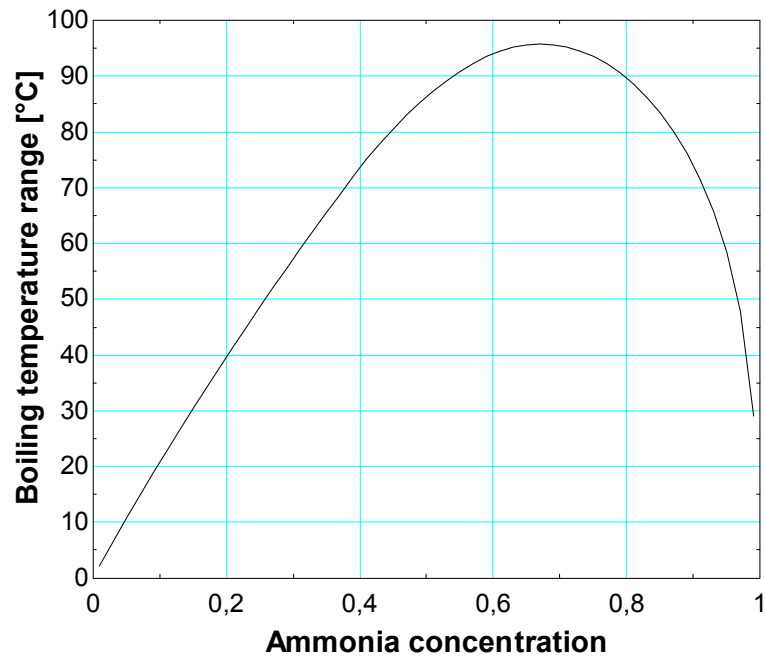


FIGURE 15: Ammonia-water boiling range at 30 bar pressure

The enthalpy of vaporization is as well dependent on the ammonia concentration (Figure 16).

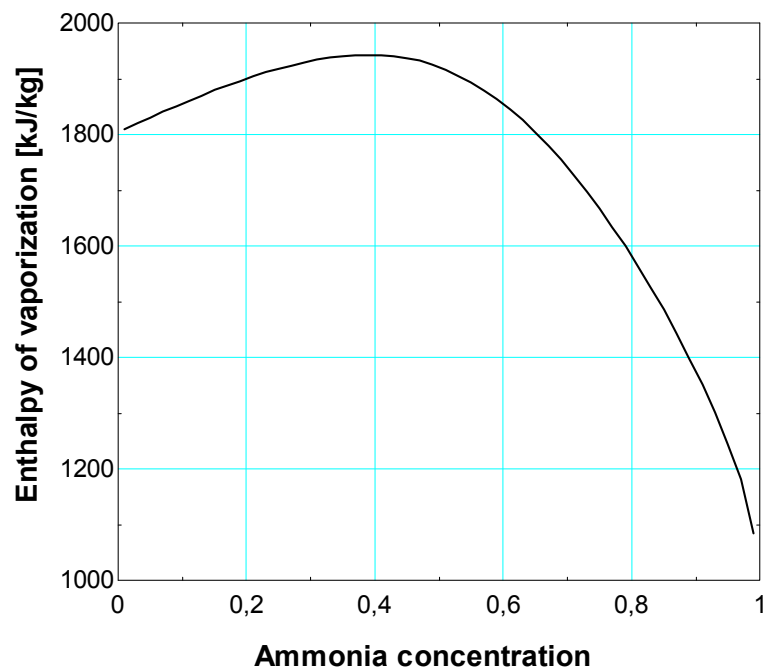


FIGURE 16: Ammonia-water enthalpy of vaporization at 30 bar pressure

Ammonia-water mixture is technically well known and widely used as a working fluid. Ammonia-water mixtures have been used in absorption refrigeration systems for decades. And ammonia is no newcomer to the technical field, it has been used in chemical and refrigeration processes for very long time. Ammonia is toxic, but the safeguards are well established.

Following are temperature - enthalpy diagrams for the mixture, at 25%, 75% and 95% ammonia concentration (Figures 16-18). The change in the curve form for boiling at constant pressure is to be noted. For low ammonia concentration, the largest temperature increase is at the beginning of the boiling, for high concentration at the end of the boiling. Intermediate concentration has S-formed boiling curve, and is therefore best suitable for power generation.

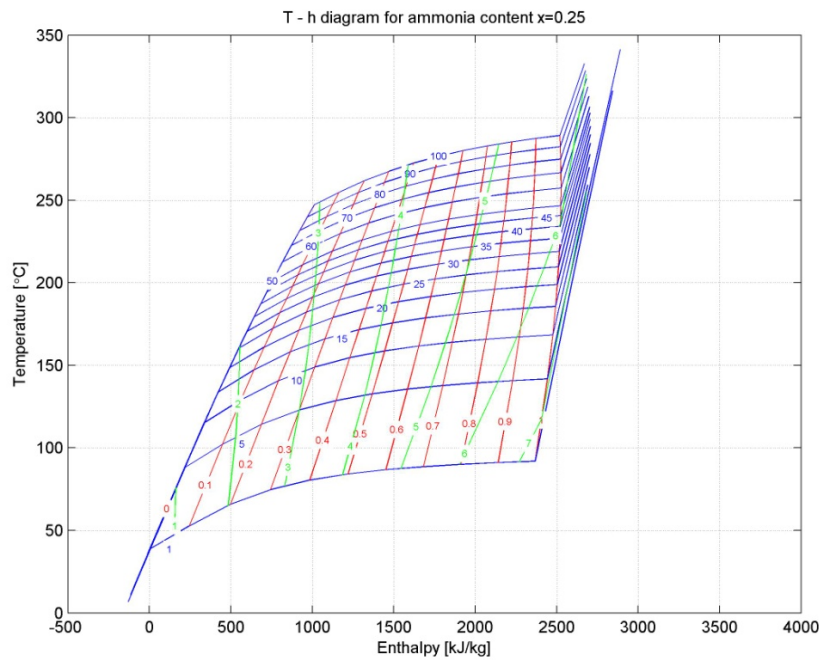


FIGURE 17: T-h diagram for 25% ammonia-water mixture

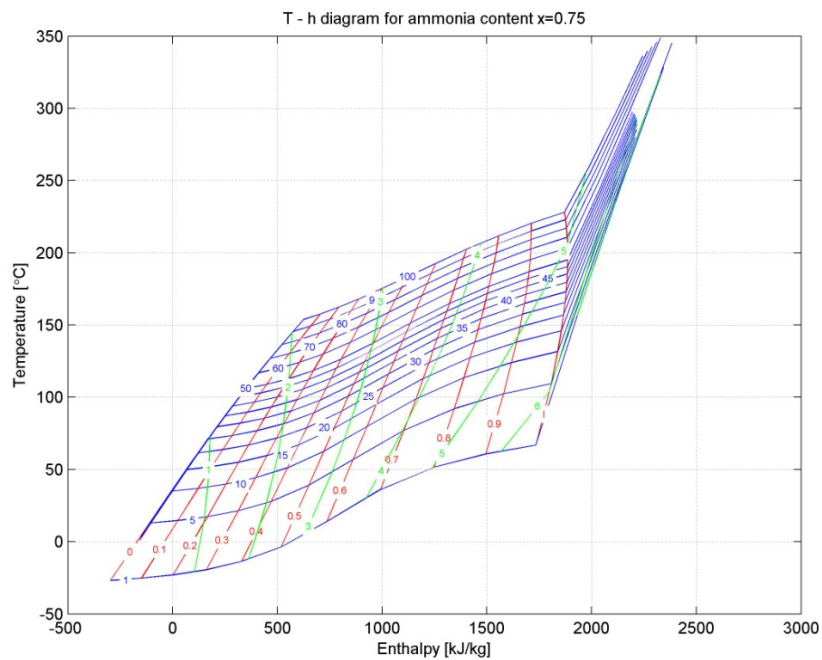


FIGURE 18: T-h diagram for 75% ammonia-water mixture

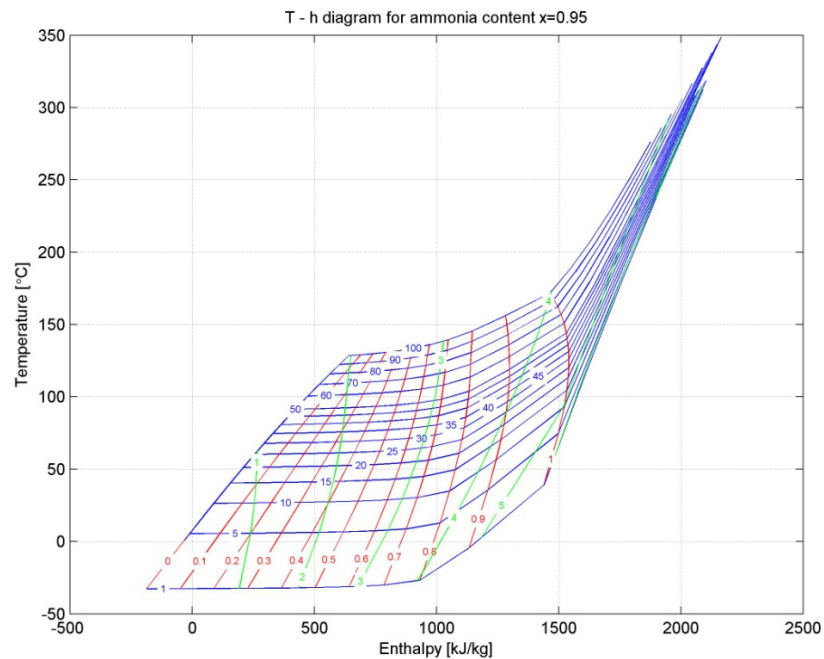


FIGURE 19: T-h diagram for 95% ammonia-water mixture

6.2 The cycle

A flow sheet for the Kalina saturated cycle is shown in Figure 20. The cycle is “saturated” because there is no superheat in the cycle. The fluid is not boiled entirely in the vaporizer, and the vapour-liquid mixture is then separated afterwards. This is done in order to maximise the vapour temperature at the vaporizer outlet.

The geothermal fluid enters the well at the source inlet temperature, station $s1$. The fluid is frequently liquid water. If the pressure is kept sufficiently high, no non-condensable gases will be separated from the liquid, and a gas extraction system is not necessary. The fluid is then cooled down in the vaporizer, and sent to re-injection at station $s2$.

Pre-heated (in the regenerators) liquid ammonia-water mixture enters the vaporizer at station 3. The fluid is boiled partly in the vaporizer. The liquid-vapour mixture leaves the vaporizer at station 4, and enters the separator.

The separated liquid leaves the separator and enters the high temperature regenerator at station 7. After the high temperature regenerator the liquid is throttled down to the condenser pressure in station 8, and mixed with the turbine exit vapour from station 6.

The ammonia-rich vapour enters the turbine at station 5, and is expanded to the condenser pressure at station 6. The exit vapour mixed with the throttled liquid (now at the average ammonia concentration) from the high temperature regenerator enters the low temperature regenerator at station 9.

The cooled fluid from the low temperature regenerator enters the condenser at station 10. The fluid gas now started to condense, and the ammonia concentration is not the same in the liquid or vapour phase. An absorption process is going on, where the ammonia rich vapour is absorbed into the leaner liquid, in addition to condensation due to lowering of the mixture temperature. The kinetics of the absorption process determines the rate of absorption, whereas heat transfer and heat capacity controls the condensation process.

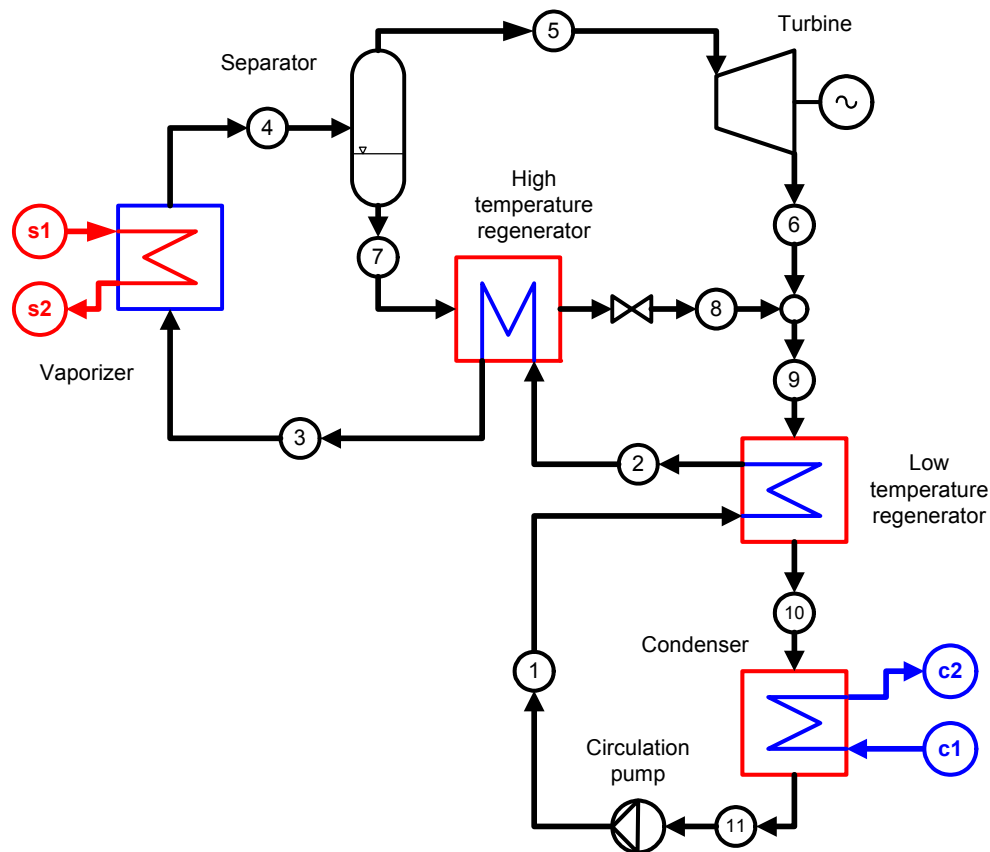


FIGURE 20: Flow diagram of a saturated Kalina cycle

Finally all the mixture is in saturated liquid phase in the hot well of the condenser at station 11. The circulation pump raises the fluid pressure up to the higher system pressure level, and the liquid is then preheated in the regenerators in stations 1 through 3.

The condenser shown here is water cooled, with the cooling water entering the condenser at station $c1$ and leaving at station $c2$.

6.3 External heat exchange

A mixture of ammonia and water will not boil cleanly, but as well change the chemical composition. The vapour will be more ammonia – rich, whereas the liquid will be leaner for the partially boiled mixture. This can be seen from the phase diagram of ammonia –water mixture presented earlier. Similar variation of the chemical composition will be encountered in the condenser for the partially condensed mixture. This results in a variable temperature during the heat exchange process both in the vaporizer and the condenser. Following is a heat exchanger diagram for a vaporizer, where typical curves have been drawn both for isopentane and 80% ammonia – water mixture (Figure 21).

The temperature difference between the primary and the secondary fluid in the Kalina vaporizer is small compared for the isopentane vaporizer, even for similar or same pinch temperature difference. Entropy is generated whenever heat is transferred over a finite temperature difference, thus is the entropy generation in the Kalina vaporizer less, and thereby the destruction of exergy less. On the other hand the Kalina vaporizer will need larger heat exchange area due to the smaller temperature difference. And the diagram shows well that the logarithmic temperature difference approach for the sizing cannot be used, as the fluid heat capacity is far from being constant.

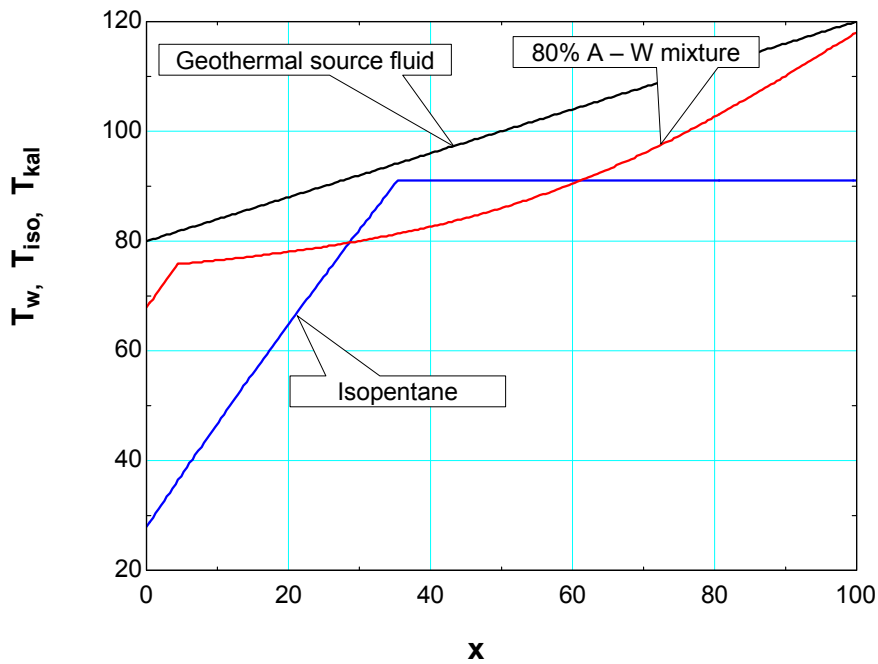


FIGURE 21: Heat exchanger diagram for a vaporizer in a binary power plant $x=100$ is at geothermal fluid entry, and $x=0$ at the outlet

A similar situation is in the condenser. There ammonia rich vapour is absorbed and condensed, with the associated changes in chemical composition of both liquid and vapour. Following is a heat exchanger diagram of both isopentane and ammonia – water mixture in a water cooled condenser (Figure 22).

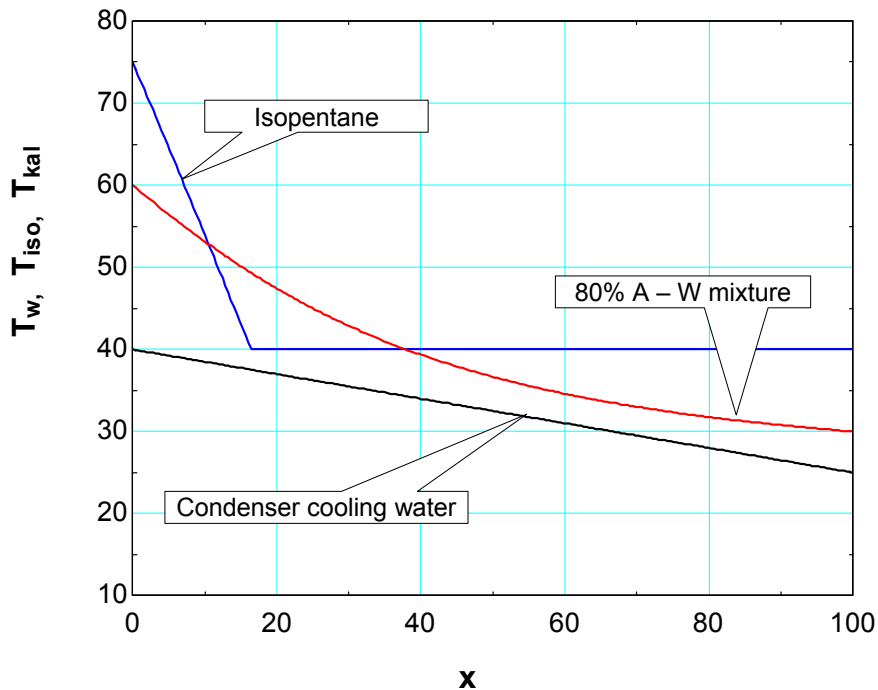


FIGURE 22: Heat exchanger diagram for a condenser in a binary power plant $x=100$ is at cooling water entry, and $x=0$ at the outlet

Both fluids will have the pinch point internally in the condenser, and the ammonia – water mixture will even have the pinch at an unknown point. The isopentane will obviously have the pinch at the fluid dew point, but it cannot be known beforehand at which vapor ratio the pinch for the ammonia – water mixture will be.

6.4 Kalex / New Kalina

A novel cycle has been invented by Mr Kalina, using ammonia – water mixture as well. Information on this cycle is sparse, and no commercial application is presently known. It seems that Mr Kalina is employing more pressure stages in the new cycle, resulting in that the mixture concentration in the cycle can be better optimized. That means as well that there are more concentration variations in the cycle. Time will show if the increased complexity of this cycle proves to be worth the claimed increase in efficiency.

7. COMBINED CYCLES

The cycles treated previously are frequently combined. A binary cycle is then used as a bottoming cycle to a flash cycle, increasing the total plant efficiency at the cost of complexity. The flash cycle has the benefit of low investment, and the binary bottoming cycle serves then to increase the efficiency – for substantially increased investment cost.

Samples of two such combinations are shown in Figures 23 and 24.

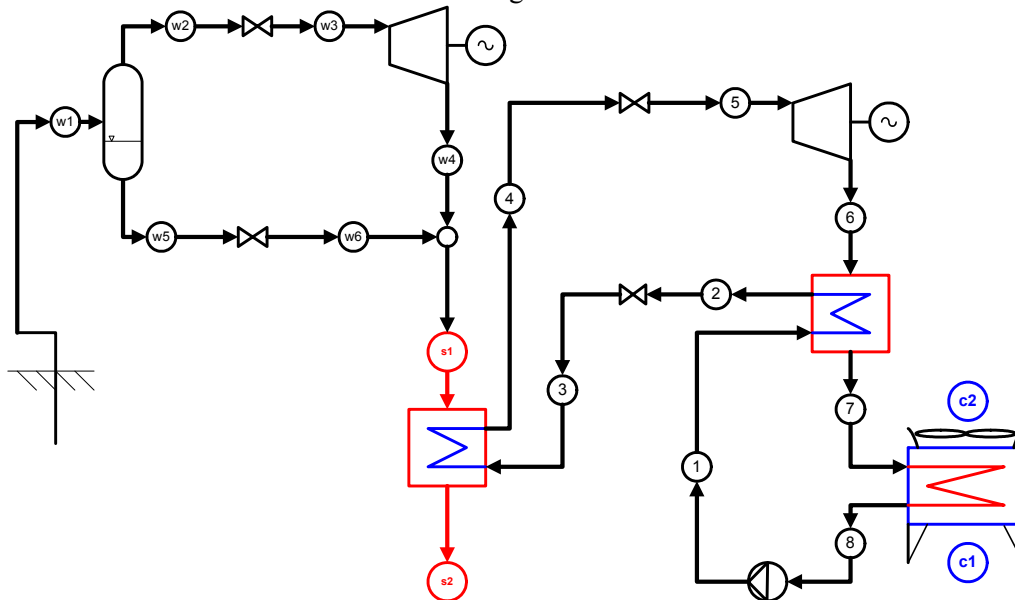


FIGURE 23: A single flash back pressure cycle combined with an ORC cycle

8. CYCLE COMPARISON

The flash steam cycles require high enthalpy of the geothermal fluid to be feasible. The fluid is separated, which can lead to chemical problems with the brine, when the mineral concentration increases due to the flashing. All non-condensable gas released from the fluid in the flashing process will have to be removed from the condenser (if present) and disposed of in an environmentally sound way. This has limited the use of flash cycles to the high temperature geothermal fields in sparsely populated areas.

The binary cycles have the benefit of having heat exchange only with the geothermal fluid. The geothermal fluid can then be kept under sufficiently high pressure during the heat exchange process to avoid boiling and release of non-condensable gases. The fluid can then be re-injected back into the reservoir, containing all minerals and dissolved gases.

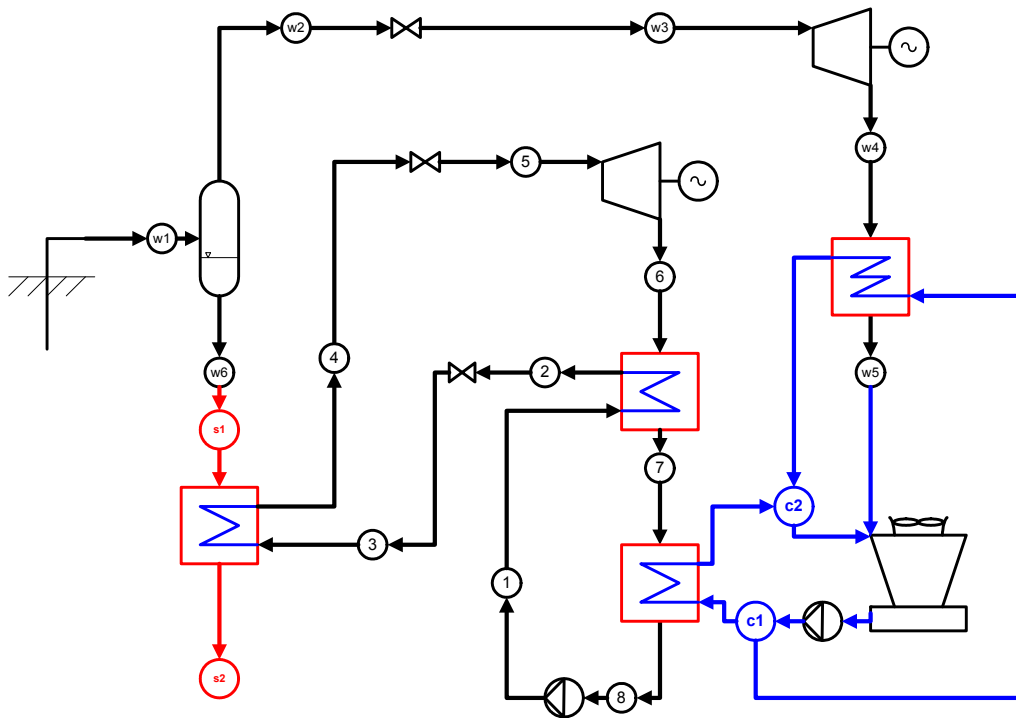


FIGURE 24: A single flash condensing cycle combined with an ORC cycle

By appropriate selection of working fluid, the geothermal fluid can be economically cooled further down than what is possible with the flash cycles. This will increase the power plant effectiveness at the cost of efficiency, as previously said. But at the end an optimum value for the plant return temperature of the geothermal fluid emerge, and this temperature will give the highest power plant output for a given flow stream from the wells.

The binary cycles have the disadvantage of having a secondary working fluid, often expensive, toxic and flammable. This leads to expensive safety measures required for the power plant.

When the geothermal fluid temperature is medium to low, the ORC cycle becomes more economical than the flash cycles. If the fluid temperature is below say 180°C it is likely that an ORC cycle will be more economical than a flash cycle. This is as well valid for higher temperatures if the gas content in the fluid is high.

The ORC cycle gives normally high power plant effectiveness. The cycle can be modified by adjusting the level of regeneration to suit the secondary process requirements (such as bottoming district heating system) or chemical limitations regarding the plant geothermal fluid return temperature. When regeneration is used, the plant efficiency increases and the plant effectiveness is reduced, as discussed before.

Another advantage of the ORC cycle is that it can be easily adapted to fluid with partial steam. The constant vaporizer boiling temperature has then to fit with the condensation temperature of the partial steam in the geothermal fluid.

When the geothermal fluid temperatures get lower than say 150-160° the Kalina cycle seems normally to be superior to the ORC cycle. Kalina is better fit for situations where the geothermal fluid is only liquid water, due to the variable temperature of the vaporizer boiling and separation process in the ammonia – water mixture.

Other technical differences between these two binary cycles are that the pressure level of the Kalina cycle are higher than for a corresponding ORC cycle. The turbine cost in the ORC cycle is thus higher, due to high volume flow in the turbine at lower pressure. On the other hand, then all equipment in the Kalina cycle will have a higher pressure class than in the ORC cycle. The piping dimensions will be larger in the ORC cycle due to higher volume flow.

There does not seem to be any major difference in requirements of the piping/equipment material for these two cycles, with the exception of the turbine. Turbine corrosion has been encountered in the Kalina cycle, leading to the use of titanium as material for the turbine rotor.

Fluid safety measures are similar, as the ORC cycle uses commonly flammable working fluids. The precautions needed due to the flammability seem to be at the same order of magnitude as the requirements due to the toxicity of ammonia.

The technical complexity of the two cycles is at the same order of magnitude. The complexity is highly dependent on the level of regeneration used in the cycle, and therefore a comparison of the cycle complexity has to be made with caution. Obviously a non-regenerated ORC cycle is a lot less complex than a highly regenerated Kalina cycle with two temperature levels of regeneration. But this is not a fair comparison.

At the time of writing this text, the only geothermal Kalina plant is at Husavik, Iceland. A second plant is being built at Unterhaching in Bavaria, Germany. Presently the limited use of the Kalina cycle may be its biggest disadvantage, but this will most probably change during the coming years. ORC cycles are widespread and have been in use for decades.

9. POWER PLANT COMPONENTS

This chapter treats the main equations and short discussion of the main power plant components. The most relevant items related to geothermal engineering are as well discussed shortly.

9.1 Well and separator

A simplified model of the well and separator is presented in Figure 25. Station 1 is the undisturbed geothermal reservoir. The main thermal parameter for the reservoir with regard to the power plant

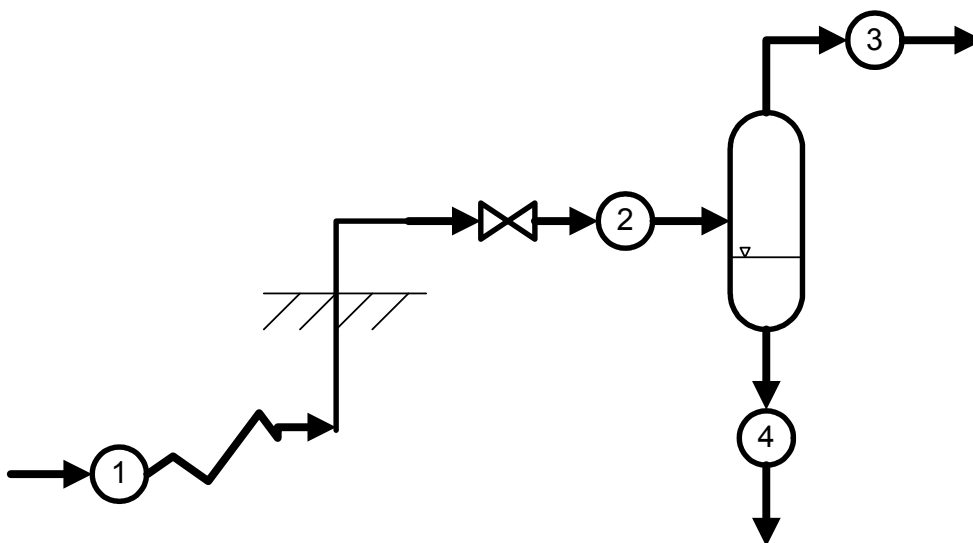


FIGURE 25: A simple model of well and separator

design is the field enthalpy, or energy content of the fluid. Station 2 is the entry of the steam – water separator, station 3 is the steam outlet from the separator and station 4 is the brine outlet of the separator.

The wells have certain productivity, i.e. there is a relation between the wellhead pressure and the flow from the well. The productivity is individual from well to well, and this relation is further complicated by the fact that the well may not be artesian, that is a well pump is required to harvest fluid from the well. Generally this relation can be presented as:

$$\dot{m}_1 = f(p_2) \quad (1)$$

where the function takes the presence of a well pump into account, as well the field characteristic.

The flow up the well and in the geothermal primary system can usually be treated as isenthalpic, the is that the heat loss in the well and the piping is neglected. No fluid loss is assumed, leading to:

$$\dot{m}_2 = \dot{m}_1 \quad (2)$$

$$h_2 = h_1 \quad (3)$$

The throttling in the well and primary system results most frequently in that the fluid starts to boil, which results in that the temperature is a direct function of the separator pressure (Station 2). If the well is non-artesian and a well pump is used, the pressure may be kept sufficiently high to avoid boiling, in which case a separator is not needed at all and the source fluid is liquid in the sub-cooled region at all times.

If boiling occurs and a separator is employed, the relation between temperature and pressure is:

$$T_2 = T_{sat}(p_2) \quad (4)$$

defined by the thermodynamic properties of steam and water.

The steam fraction is then defined by the energy balance over the separator. The heat flow in the incoming mixture of steam and water (from the well) equals the sum of the energy flows in the steam and the brine from the separator. The mass flow of steam from the separator will thus be:

$$\dot{m}_3 = \dot{m}_2 \frac{h_2 - h_4}{h_3 - h_4} \quad (5)$$

The separator is working in the (thermodynamic) wet area, containing a mixture of steam and water in equilibrium. All temperatures in the separator will thus be equal, assuming that there are no significant pressure losses or pressure differences within the separator.

$$T_3 = T_2 = T_4 = T_{sat}(p_2) \quad (6)$$

The enthalpy of the steam outgoing stream from the separator is thus the enthalpy of saturated steam at the separator pressure.

$$h_3 = h_g(p_2) \quad (7)$$

Mass balance holds over the separator, the sum of steam mass flow and brine mass flow equals the mass flow of the mixture from the wells towards the separator.

$$\dot{m}_4 = \dot{m}_2 - \dot{m}_3 \quad (8)$$

The selection of separator pressure is very critical for the power plant. If the wellhead pressure is low, boiling may occur in the formation around the well, which may lead to scaling within the cracks and narrow flow passages in the formation. This will lead to short well life.

Higher separator pressure means that better steam is available for the turbine (higher enthalpy), but the amount will be less, dictated by the separator energy balance as well as less well productivity due to higher wellhead pressure. This may as well influence the separation of non-condensable gases from the geothermal fluid.

The selection of the separator pressure is thus an optimization process, economical, thermodynamic and geothermal.

9.2 Vaporizer

The vaporizer is the first component of an ORC or a Kalina power plant (Figure 26). Station s1 is the entry of the geothermal fluid to the vaporizer, and station s2 is the outlet. Station 1 is the entry of the power plant working fluid (liquid) to the vaporizer, and station 2 is the outlet of the working fluid vapour or mixture towards the turbine.

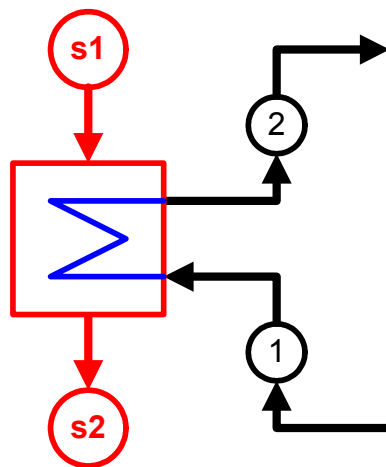


FIGURE 26: ORC vaporizer schematic

Obviously the heat removed from the source fluid has to equal the heat added to the working fluid.

$$\dot{m}_s (h_{s1} - h_{s2}) = \dot{m}_{working\ fluid} (h_2 - h_1) \quad (9)$$

The fluid condition at station 2 is determined by the cycle and the turbine requirements, for an ORC cycle this would be saturated or slightly superheated, for most Kalina cycles it would be in the wet region, with vapor fraction at 50-100%.

The vaporizer is nothing but a heat exchanger between the hot source fluid and the cold working fluid of the cycle. It has to be observed that the temperature of the hot fluid is higher than the one of the cold fluid throughout the vaporizer. As well it must be kept in mind that the relation between the

enthalpy and the temperature is highly non-linear, requiring that the vaporizer is divided into appropriate sections for the calculation.

The source fluid outlet temperature is critical as regards scaling. This temperature must be kept sufficiently high to avoid scaling on the source fluid side of the exchanger. Cleaning of the source fluid side may be necessary, so the vaporizer design must take this into account. Any geothermal fluid may be corrosive, so an appropriate material has to be used for the vaporizer.

9.3 Turbine

The turbine converts a part of the vapour enthalpy to shaft work, and then electricity in the generator (Figure 27). Station 1 is the vapour inlet to the turbine, and station 2 is the turbine exit.

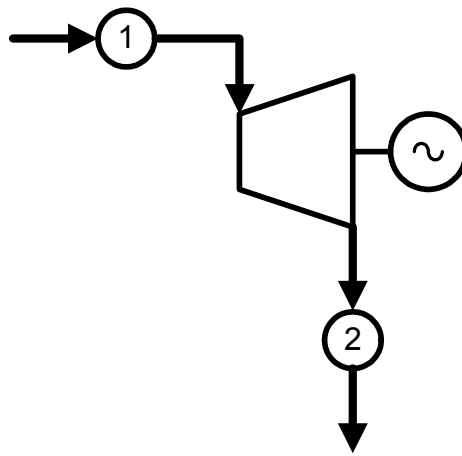


FIGURE 27: Turbine schematic

The ideal turbine is isentropic, having no second law losses. In this case the entropy of the incoming vapor equals the entropy in the exhaust steam. The corresponding enthalpy change (reduction) of the vapor is the largest enthalpy change possible. The isentropic exit enthalpy is then the enthalpy at the same entropy as in the inlet and at the exit pressure, which is roughly the same as prevails in the condenser.

$$h_{2,s} = h(s_1, p_2) \quad (10)$$

The turbine isentropic efficiency is given by the turbine manufacturer. This efficiency is the ratio between the real enthalpy change through the turbine to the largest possible (isentropic) enthalpy change. The real turbine exit enthalpy can then be calculated:

$$h_2 = h_1 - \eta_{is}(h_1 - h_{2,s}) \quad (11)$$

The work output of the turbine is then the real enthalpy change multiplied by the working fluid mass flow through the turbine.

$$\dot{W} = \dot{m}(h_1 - h_2) \quad (12)$$

The expansion through the turbine may result in that the exit vapor is in the wet region, or that a fraction of the mass flow is liquid. This can be very harmful for the turbine, resulting in erosion and blade damage.

The Kalina cycle uses a mixture of ammonia and water, so that the droplets created in the turbine are electrically conductive. It is the meaning of the writer that this conductivity is the reason for the corrosion encountered in the turbine in Husavik, Iceland. This corrosion has been avoided by the usage of non-magnetic titanium for the turbine rotor.

Many of the working fluids for the ORC cycle are retrograde, which means in this context that the exit vapor is superheated. The heat removal in the condenser will then partly be “de-superheat”, heat transfer out of the vapor at temperature higher than the final condensing temperature.

Ammonia-water mixture is not retrograde, but as the condensation will occur at a variable temperature, the heat removal process is very similar to that of the retrograde fluids.

9.4 Recuperator

The regenerator is a heat exchanger between the hot exit vapour from the turbine and the condenser (Figure 28). It is a de-superheater in the ORC cycle, transferring heat from the turbine exit vapour to the condensate from the condenser.

Station 1 is the turbine exit vapour, station 2 is the regenerator outlet towards the condenser, station 3 is the inlet of the condensate from the condenser, and station 4 is the pre-heated feed to the vaporizer.

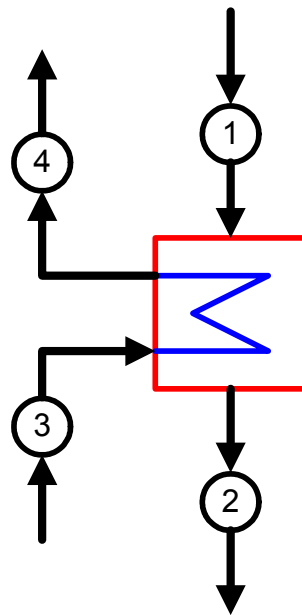


FIGURE 28: Recuperator schematic

The heat removed from the turbine exhaust vapor is equal the heat added to condensate:

$$\dot{m}(h_1 - h_2) = \dot{m}(h_4 - h_3) \quad (13)$$

The mass flow is the same on both sides of the regenerator. The hot fluid from the turbine is on the hot side, will be condensed in the condenser and then pumped right away through the cold side of the regenerator towards the vaporizer.

It has to be observed that the temperature of the hot fluid is higher than the one of the cold fluid throughout the regenerator. The fluid behavior is usually close to linear, so it is normally not necessary to divide the regenerator into sections.

The effect of regeneration on the cycle has been treated earlier in this text.

9.5 Condenser

The condenser may be either water or air cooled (Figure 29). The calculations for the condenser are roughly the same in both cases, as the cooling fluid (air or water) is very close to linear. Station 1 is the working fluid coming from the regenerator (or turbine in the case of a non-regenerated cycle). Station 2 is the condensed fluid, normally saturated liquid with little or no sub-cooling. Station c1 is the entry of the cooling fluid, station c2 the outlet.

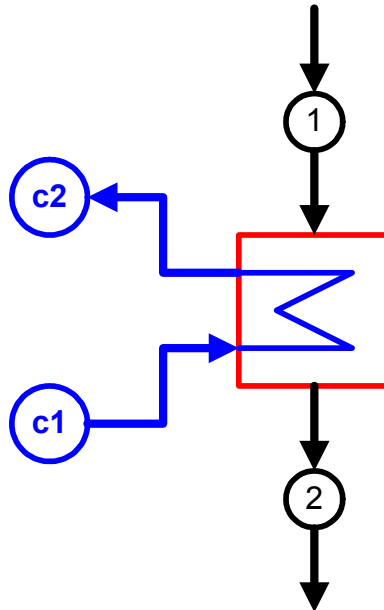


FIGURE 29: Condenser schematic

The condenser is nothing but a heat exchanger between the hot vapor from the regenerator/turbine and the cooling working fluid of the cycle. It has to be observed that the temperature of the hot fluid is higher than the one of the cold fluid throughout the condenser. As well it must be kept in mind that the relation between the enthalpy and the temperature is non-linear, requiring that the vaporizer is divided into appropriate sections for the calculation. This is especially valid for Kalina cycles, in the ORC cycle there is only a property change at the dew point, where de-superheat ends and condensation begins.

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